Amendments to the Claims

- 1. (Currently amended) A method for the purification of producing marigold oleoresin, which is characterized by carrying out a step of subjecting marigold oleoresin to supercritical fluid extraction and a step of dissolving marigold oleoresin in a ketone solvent, cooling the solution and removing the ingredient which precipitated in solution.
- 2. (Currently amended) A method for the purification of producing marigold oleoresin claimed in Claim 1, which is characterized in that a purified marigold oleoresin having a low viscosity and a high lutein content is obtained by carrying out a step of subjecting marigold oleoresin to supercritical fluid extraction and a step of dissolving marigold oleoresin in a ketone solvent, cooling the solution and removing the ingredient which precipitated in solution. isolated.
- 3. (Currently amended) A method for the purification of producing marigold oleoresin claimed in any one of Claims 1 to 2 Claim 1, which is characterized by carrying out a the step of supercritical fluid extraction in the presence of a diluent.
- 4. (Currently amended) A method for the purification of producing marigold oleoresin claimed in any one of Claims 1 to 3 Claim 1, which is characterized by using a supercritical fluid selected from the group consisting of carbon dioxide, ethane, ethylene, propane, toluene and dinitrogen monoxide.
- 5. (Currently amended) A method for the purification of producing marigold oleoresin claimed in Claim 1, which is characterized in that the ketone solvent described in Claim 1 is acetone, methylethylketone or diethylketone.
- 6. (Currently Amended) A method for the purification of producing marigold oleoresin claimed in any one of Claims 1 to 5 Claim 1, wherein the supercritical fluid extraction is carried out using a carbon dioxide supercritical fluid under the condition that the carbon dioxide pressure is $(980 \text{ to } 2940) \times 10^4 \text{ Pa}$ (=N/m²) and the temperature is at critical

temperature to 80°C.

- 7. (Currently amended) A method for the purification of producing marigold oleoresin claimed in any one of Claims 1 to 5 Claim 6, wherein the supercritical fluid extraction is carried out using a carbon dioxide supercritical fluid under the condition that the carbon dioxide pressure is $(1470 \text{ to } 2450) \times 10^4 \text{ Pa}(=\text{N/m}^2)$ and the temperature is at 40°C to 60°C.
- 8. (Currently amended) Purified marigold oleoresin obtained by a the method described in any one of Claims 1 to 7 Claim 1.
- 9. (Currently amended) Purified marigold oleoresin <u>as claimed in Claim 8</u>, having low viscosity and a high lutein content obtained by a method described in any one of Claims 1 to 7.
- 10. (Currently amended) Purified marigold oleoresin as claimed in Claim 8 which contains not less than 20% of lutein-fatty acid ester and has a viscosity of not more than 20,000 mPa.s at 30°C.
- 11. (Currently amended) Purified marigold oleoresin <u>as claimed in Claim 10</u> which contains not less than 30% of lutein-fatty acid ester and has a viscosity of not more than 20,000 mPa.s at 30°C.
- 12. (Currently amended) Purified marigold oleoresin described as claimed in Claim 11, which has a viscosity of not more than 10,000 mPa.s at 30°C.
- 13. (Currently amended) Purified marigold oleoresin described as claimed in Claim 44 12, which has a viscosity of not more than 5,000 mPa.s at 30°C.
- 14. (Currently amended) A soft capsule which contains the purified marigold oleoresin described as claimed in any one of Claims 8 to 13 Claim 8.